

VTT Technical Research Centre of Finland

Organosolv cooking as a facile fractionation method for annual plants

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VTT



Introduction of novel organosolv LGF-Process

Fractionation of Biomass

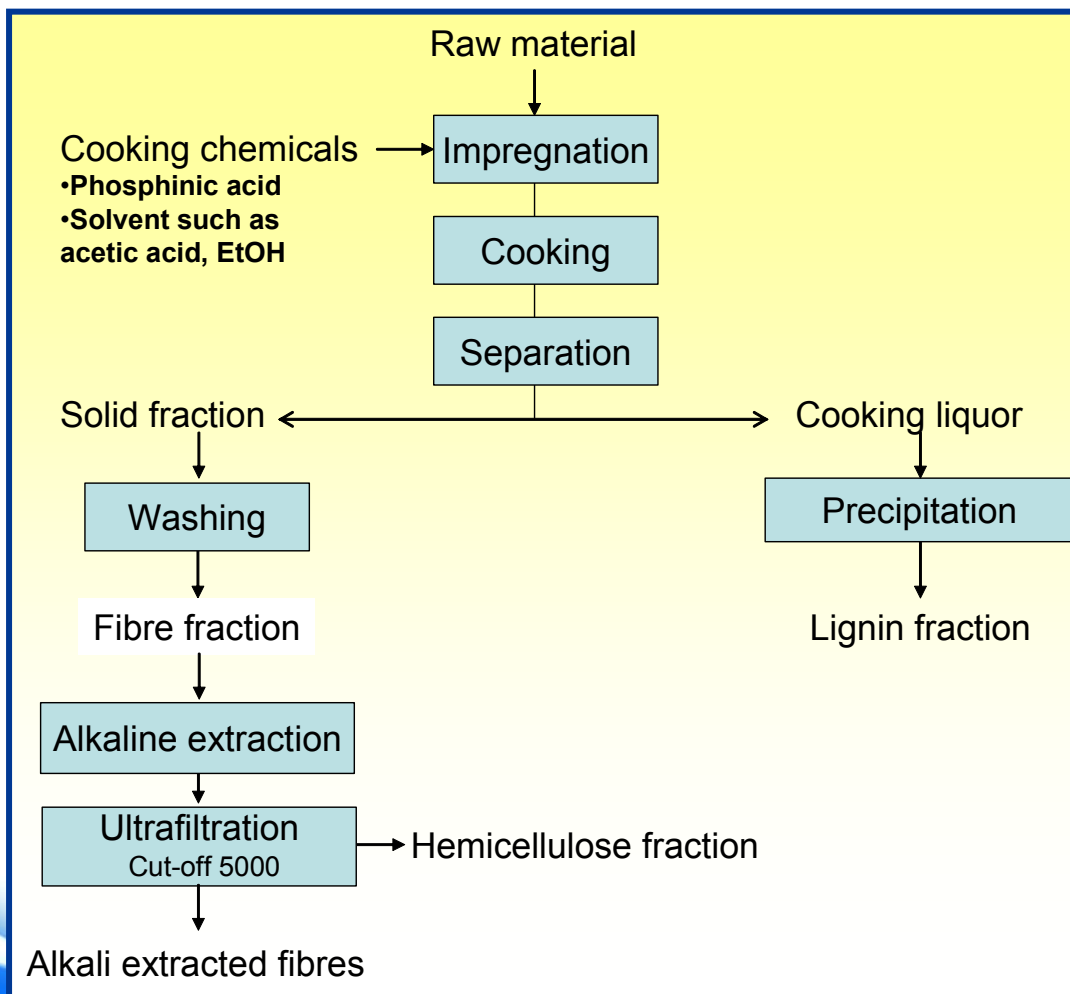


Figure 1. Schematic presentation of LGF pulping and subsequent fractionation processes

Fractionating reed canary grass by organosolv cooking

Table 1. Acetic acid/ H₃PO₂ cooking of reed canary grass

ACETIC ACID COOKING 26% moisture content of cooking liquor (CLQ)					
Sample	t °C	Time (h)	CLQ used	Fiber yield %	Hydrolysis-%
RA-1	105	4	twice	57.4	59.3
RA-2	105	8	once	54	47.8
RA-3	105	13	once	51.0	47.4
Sample	Post treatment of fiber with 1 M NaOH				
RA-1 Fiber	80	4		38	100

Symbols CLQ = Cooking liquor,
RA = Acetic acid cooking

- It is possible to use the same cooking liquor more than once (improved solid/liquid ratio)
- Complete hydrolysis of fiber is achievable when cooking is combined with alkaline extraction of fib

Fractionating reed canary grass by organosolv cooking

Table 2. Ethanol/ H₃PO₂ cooking of reed canary grass (R)

ETHANOL COOKING, 20% moisture content of cooking liquor (CLQ)					
Sample	t °C	Time (h)	CLQ used	Fiber yield	
RE-4	79	30	twice	73.5	75.8
Sample	Post treatment of fiber with 1M NaOH				
RE-4 Fiber	80	4		57	100

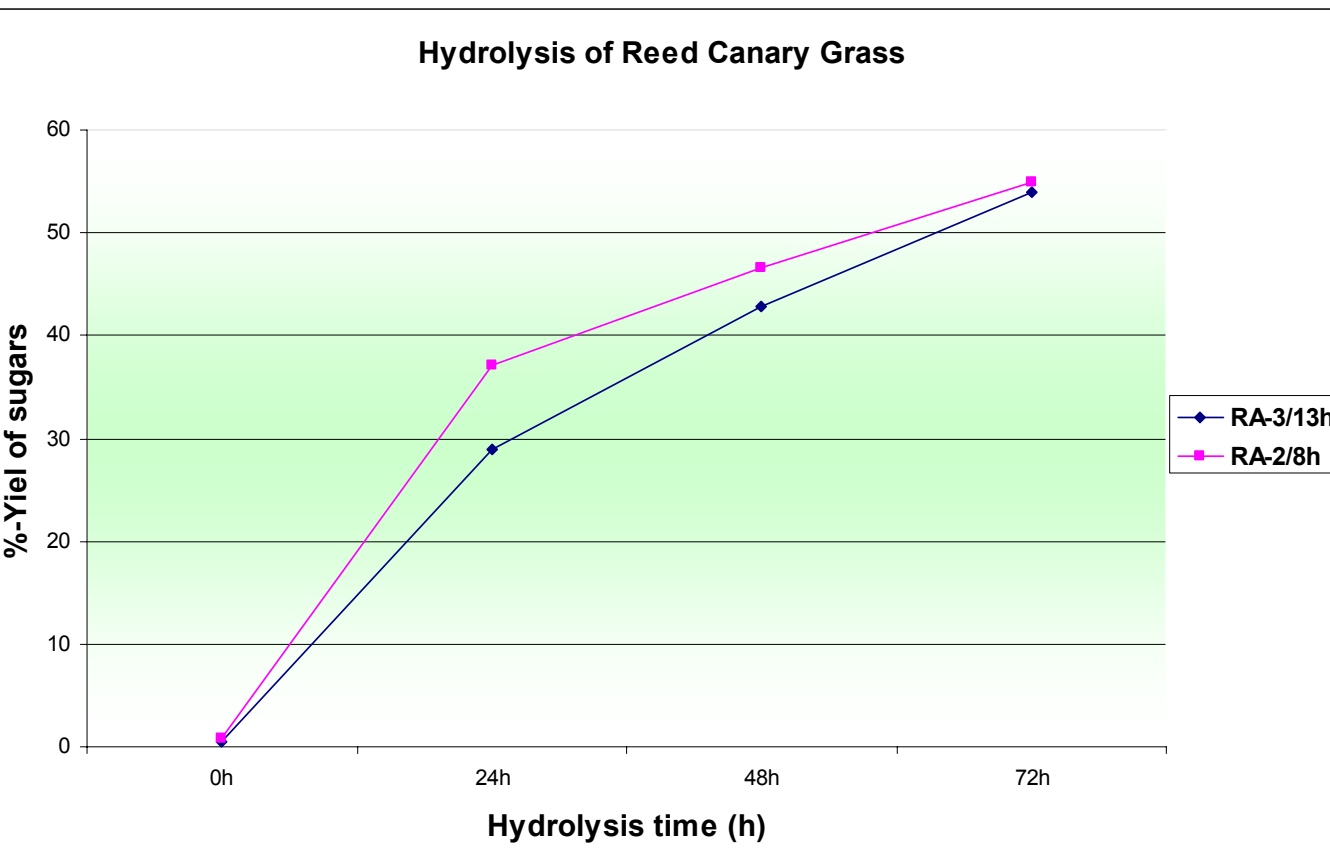
Symbols: CLQ: Cooking liquor, RE = Ethanol cooking

Table 3. Yields of isolated lignin from different cooking processes

Sample	Cooking liquid	Lignin yield % (as isolated)
RA-1	Acetic acid	13.4
RA-2	Acetic acid	21.0
RA-3	Acetic acid	11.0
RE-4	Ethanol	7.0

Very mild reaction conditions can be used for partial removal of lignin (i.e. boiling ethanol)

Enzymatic hydrolysis rate of LGF treated biomass Acetic acid cooking

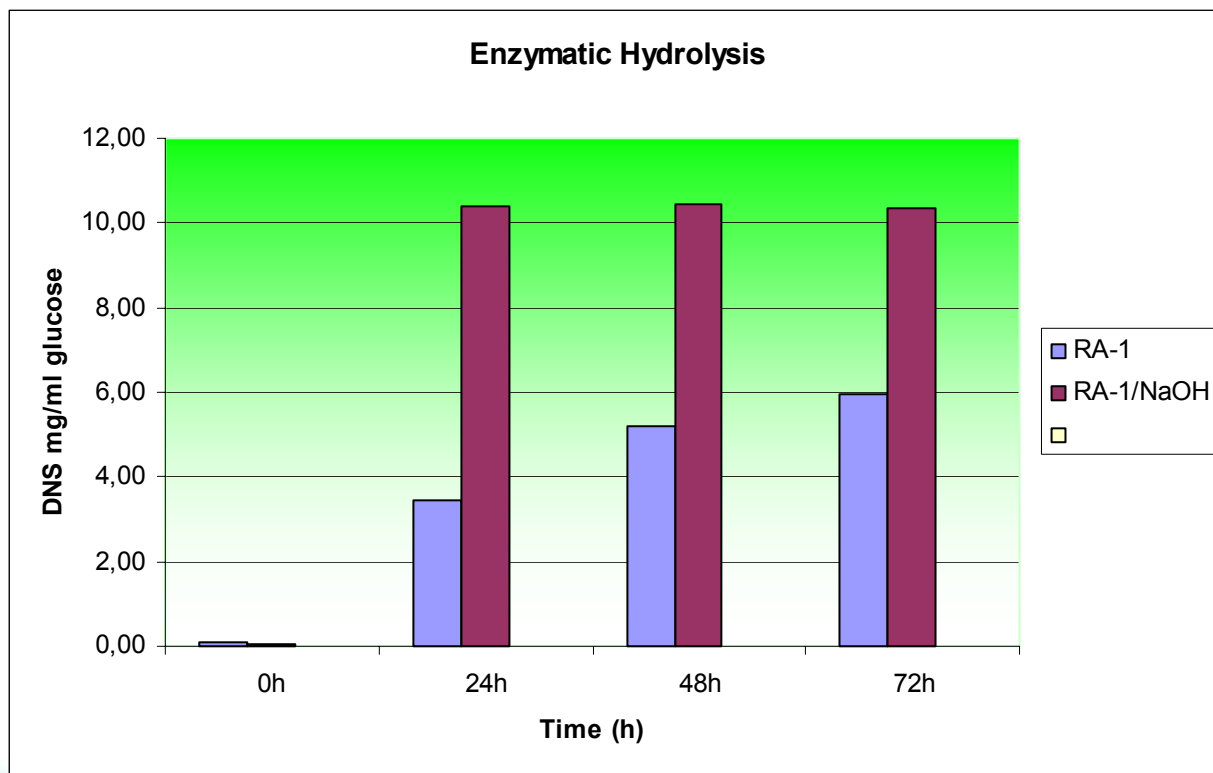


Long cooking time
does not provide any
advantage in hydrolysis

Cellulast 10 FPU/g
Novozyme 100 cat/g
10 g/l, pH5,45 °C

Figure 2. Effect of cooking time on hydrolysis rate

Enzymatic hydrolysis rate of LGF treated biomass Acetic acid cooking Fractionating



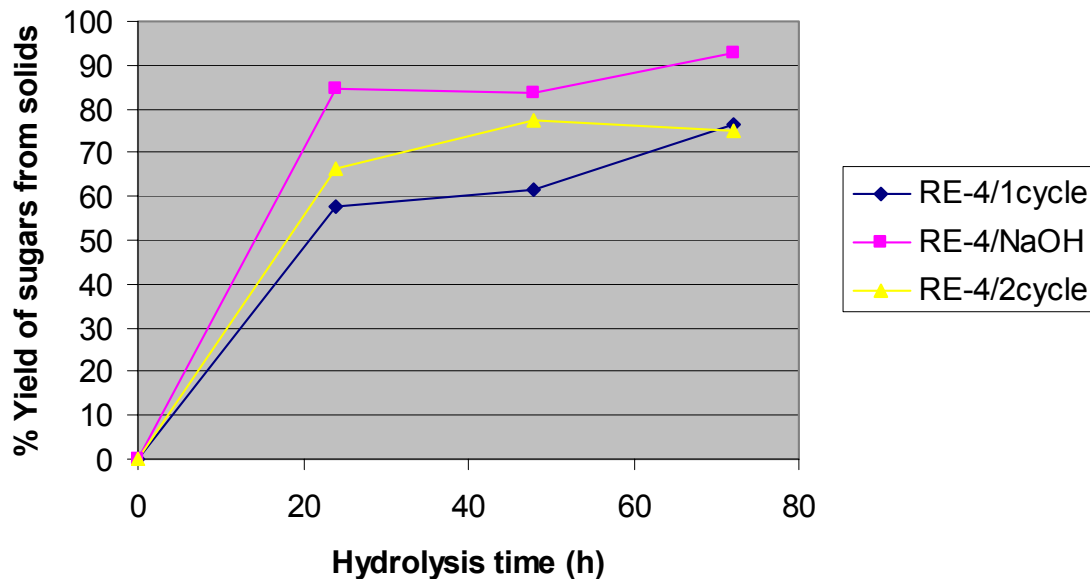
Complete hydrolysis of fiber is achieved in 24 h after fractionation and extraction with alkali

Probably alkali removes enzymatic inhibiting components from fiber (e.g hemicellulose and/or residual lignin)

Figure 3 Promoting hydrolysis rate of LGF fiber by alkaline extraction

Enzymatic hydrolysis rate of LGF treated biomass Ethanol cooking Fractionating

Hydrolysis of Reed Canary Grass

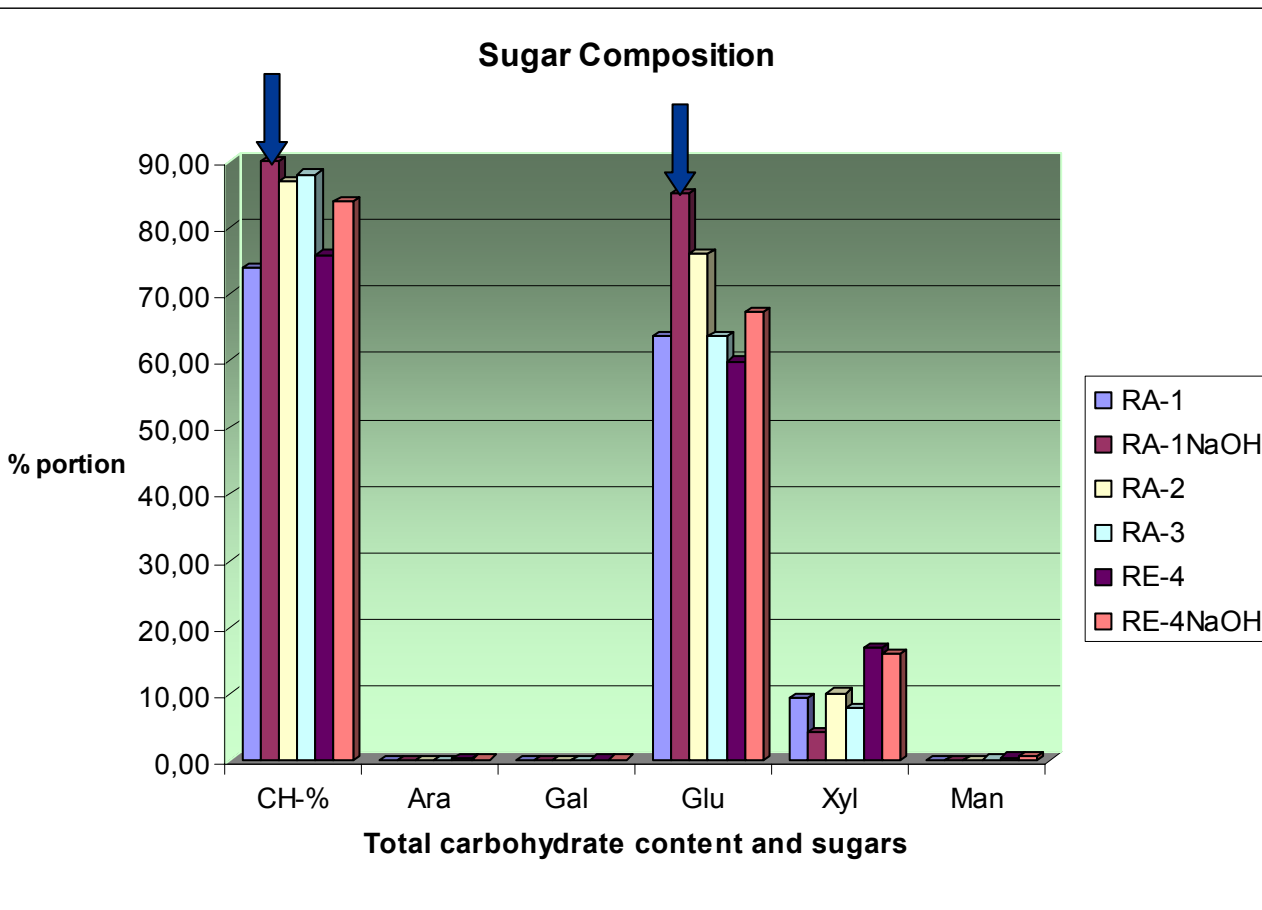


Re-usage of cooking liquor
Does not have significant
effect on hydrolysis result

Alkaline extraction increased
significantly the hydrolysis rate

Figure 4. Results from ethanol LGF cooking. Recycling of cooking liquor and removal of enzyme inhibiting components.

Carbohydrate content of fiber (reed canary grass) and distribution of individual sugars



90 % carbohydrate content obtainable (RA: acetic acid cooking)
Mainly Glu and Xyl

Portion of hemicellulose is high
Ethanol (RE) cooking, also de
amounts of arabinose, galactos
and mannose present.



NaOH extraction

Figure 5. Results from carbohydrate analysis. CH = % amount of carbohydrates of solids. Distribution (%) of individual sugars in carbohydrate part

Characterization of reed canary grass lignin NMR and DSC Results

Table 4 Background phosphorus (origin from H_3PO_2)

Lignin	at 2 ppm mmol/g	at 10- 50 ppm mmol/g	Total P mmol/g
RA	0.006	0.56	0.57
RE	0.041	0.35	0.39

Table 5 Amount of OH group species (mmol/g) in reed canary grass dissolved lignin

Lignin	Aliphatic OH	Aromatic OH	S+C	G	H	Carboxylic acid	Total OH
RE	3.3	1.8	0.4	0.8	0.6	0.3	5.4
RA	1.9	2.4	0.8	0.9	0.7	0.6	4.9

Table 6. Thermoplasticity of lignin

Lignin	Glass transition / °C	
	1. cycle	2. cycle
RE	65	61
RA	104	102
Protobind 1000, Reference	107	105

S+C = syringyl +condensed phenolic units
G = Guaiacyl unit
H = para-hydroxyphenyl phenolic unit

Conclusions

In addition to ethanol production, LGF-method is potential for fractionating lignocellulose materials to technically useful biopolymers in good overall yield.

Thank you for your attention

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