

# Lignocellulosic biomass for the production of platform chemicals – economic and ecological assessment of a biorefinery concept

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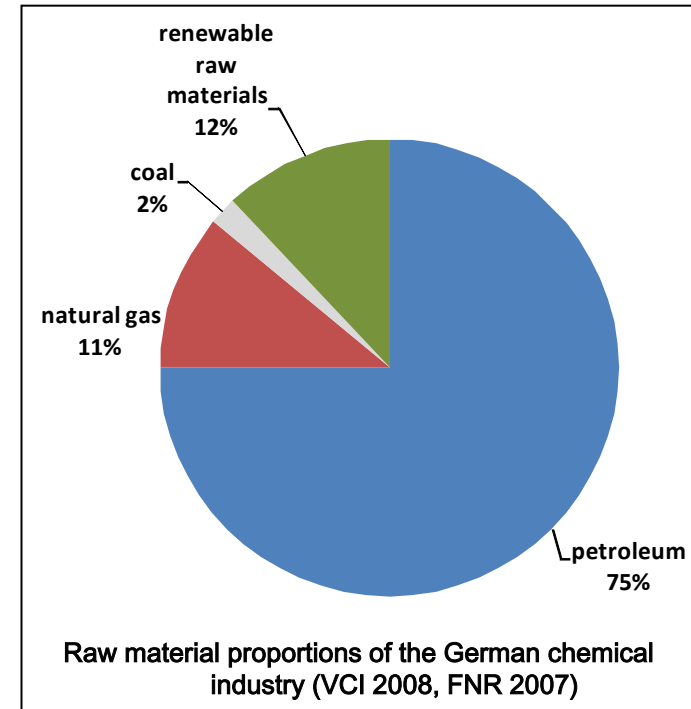


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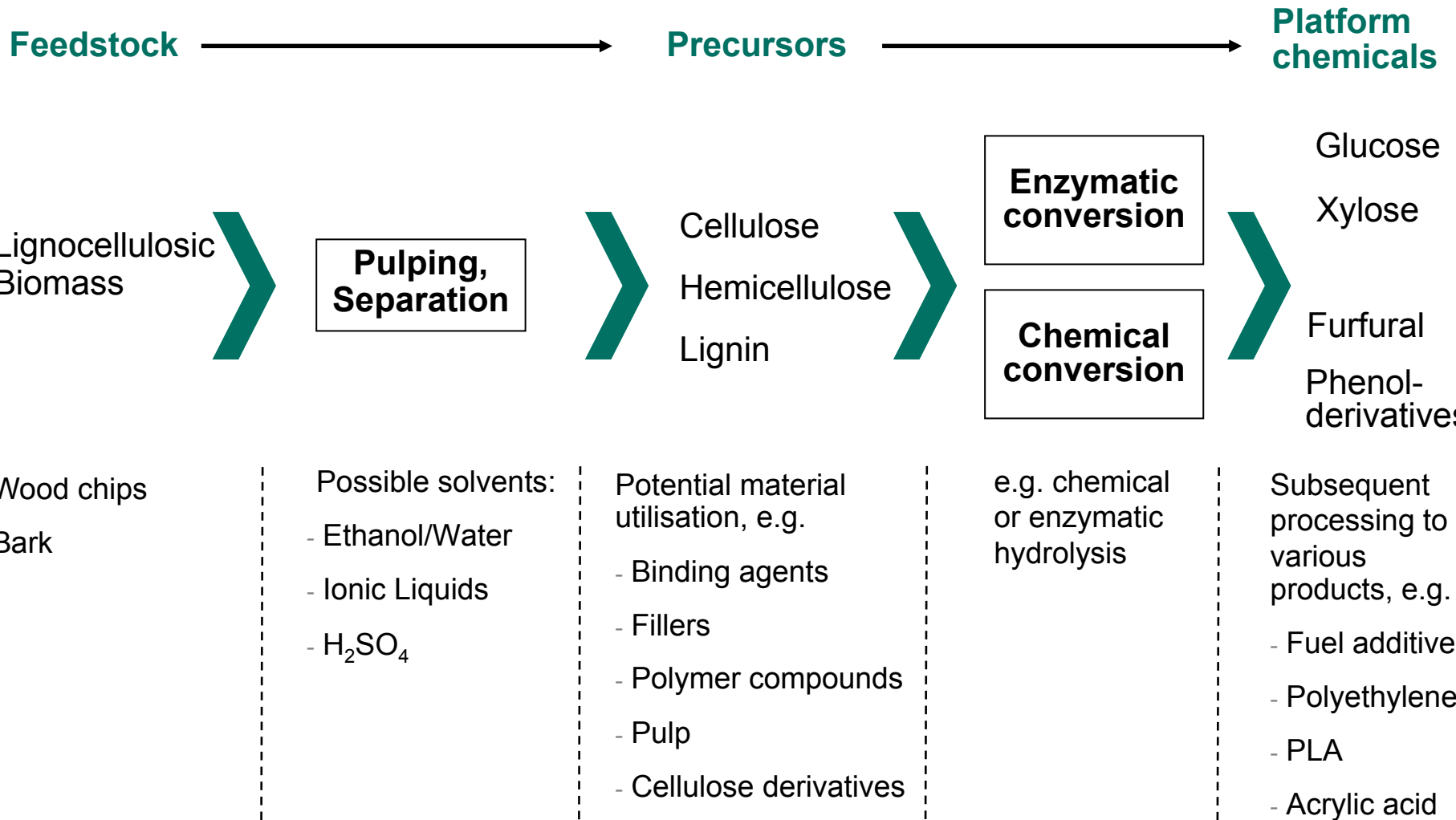
- Introduction
- Methodology for the assessment of process chains for biomass utilization
- Reference configuration of the modelled wood biorefinery
- Modelling of material and energy flows along the whole value chain
- Economic assessment of the wood biorefinery
- Ecological assessment of the wood biorefinery
- Summary

- Ca. 2 million t of renewable raw materials are currently used in the chemical industry in Germany per year
- Currently especially vegetable oils, starch and animal fats are used for the production of e.g. tensides, polymers, lubricants
- Prospective use of lignocellulosic biomass for the production of platform chemicals and new materials
- Reduction of dependency on crude oil imports and securing of raw material supply



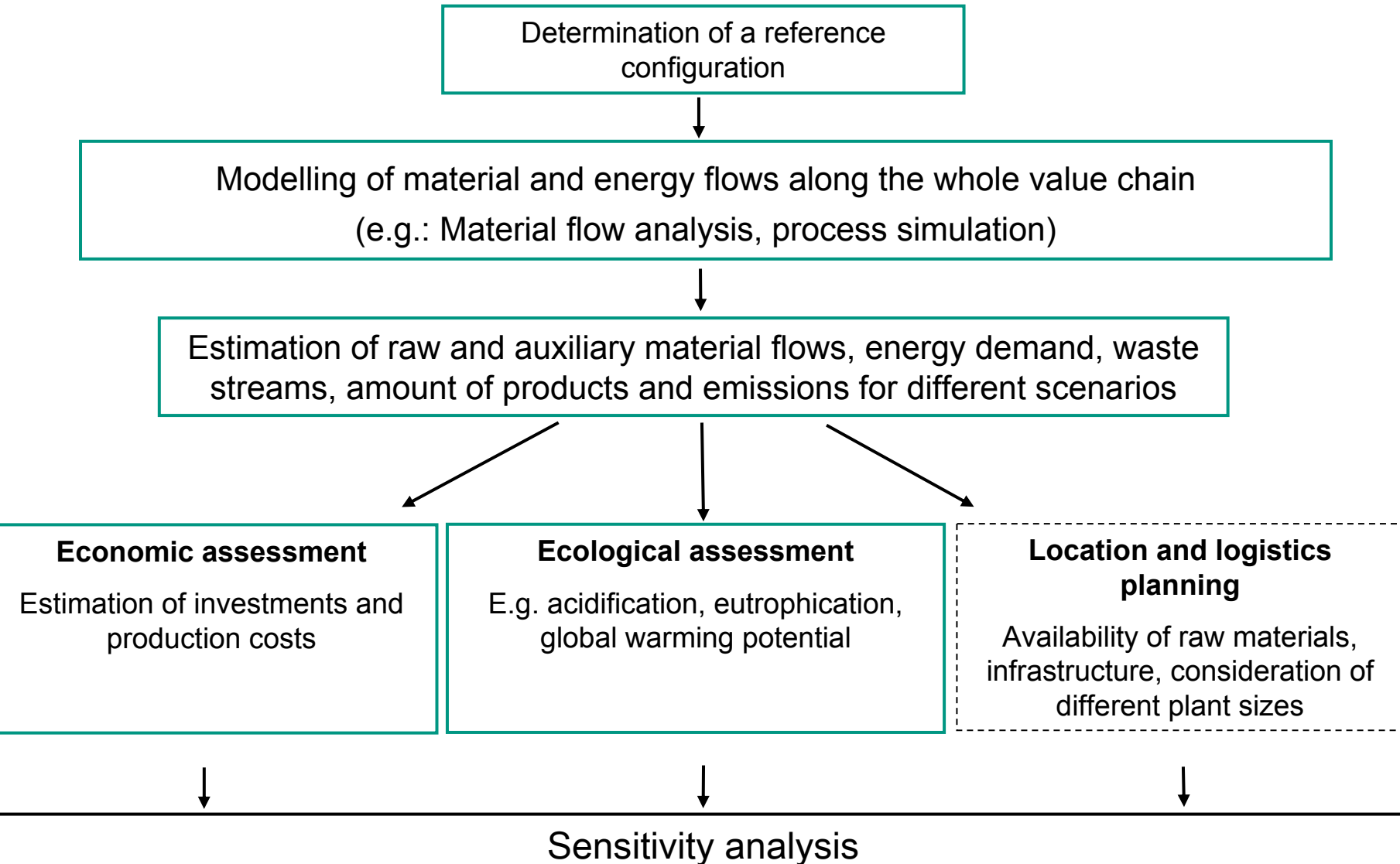
⇒ Enhancement of research and development regarding new biomass conversion technologies

# Platform chemicals from lignocellulosic biomass (examples)



- Estimation of costs and environmental effects for the production of glucose, xylose and lignin from wood along the whole value chain
- Determination of economic and ecological key parameters
- Identification of cost-effective and environmentally sound process configurations at an early stage of process development

# Methodology for the evaluation of process chains

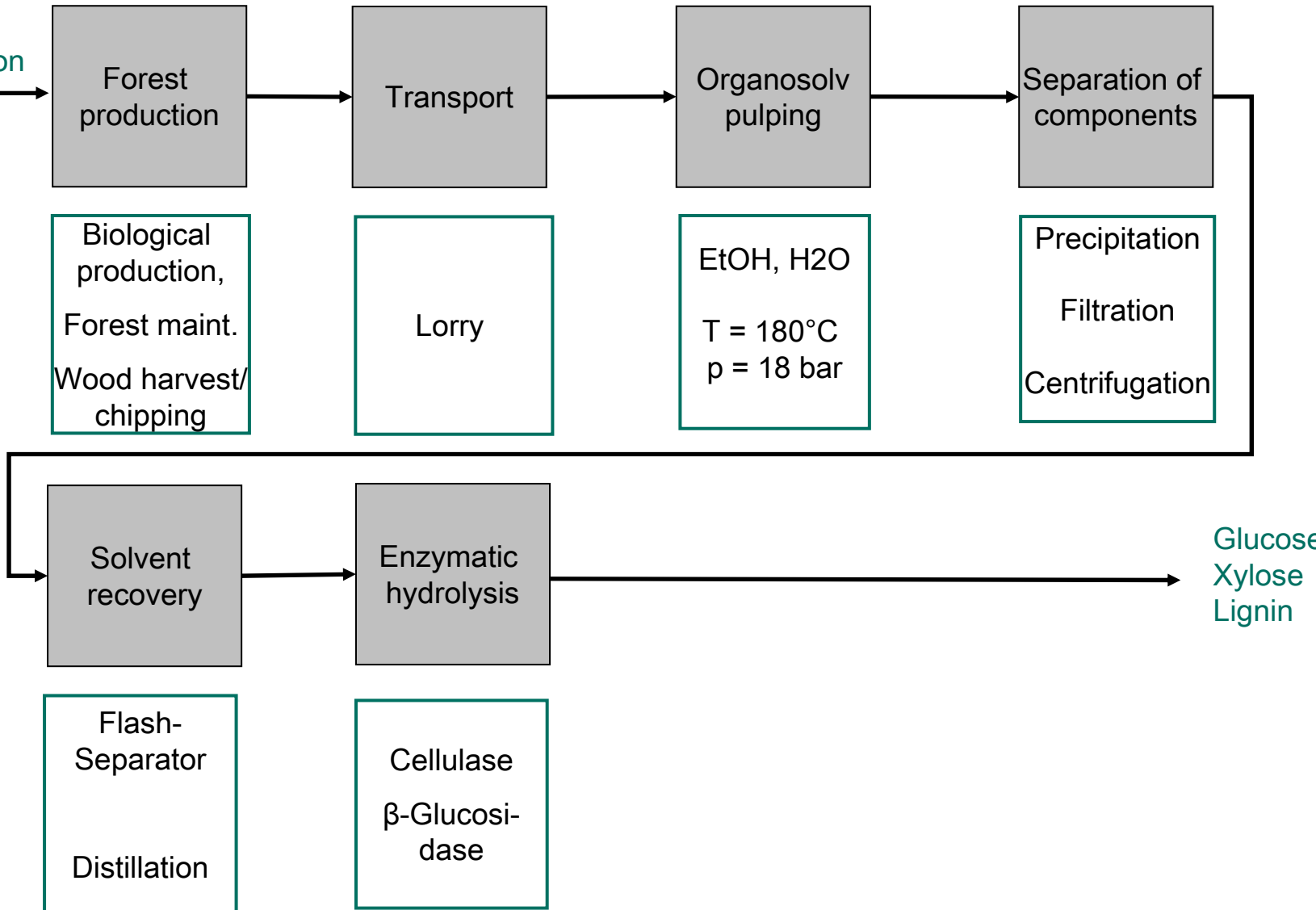


# Reference configuration of the modelled biorefinery

- Framework: Research project „Pilotprojekt Lignocellulose Bioraffinerie“
- Plant capacity: 400.000 t dry wood/year
- Load: 50 t dry wood/h (8000 h/year)
- Feedstock properties : Wood chips of residual wood (50% water content)
- Organosolv pulping: Ethanol/water solvent (50/50)  
Ratio wood : solvent = 1 : 6
- Enzymatic conversion of cellulose: Conversion rate to glucose: 82%
- Hemicellulose fraction: Solute hemicellulose fragments after organosolv pulping are subsumed to xylose
- Final products: Main product: Glucose (solution ~16 mass-%),  
Byproducts: Xylose (solution ~5 mass-%), lignin (dry)

# Major process steps for the production of glucose from wood

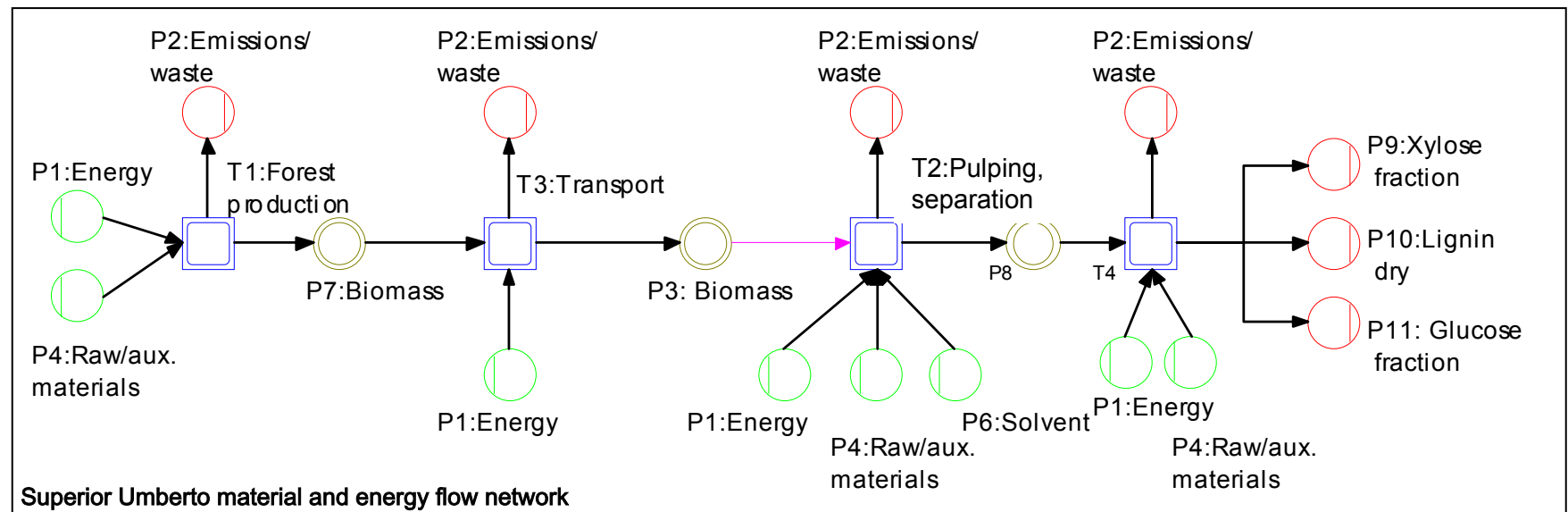
$\text{CO}_2$ ,  $\text{H}_2\text{O}$ ,  
solar radiation





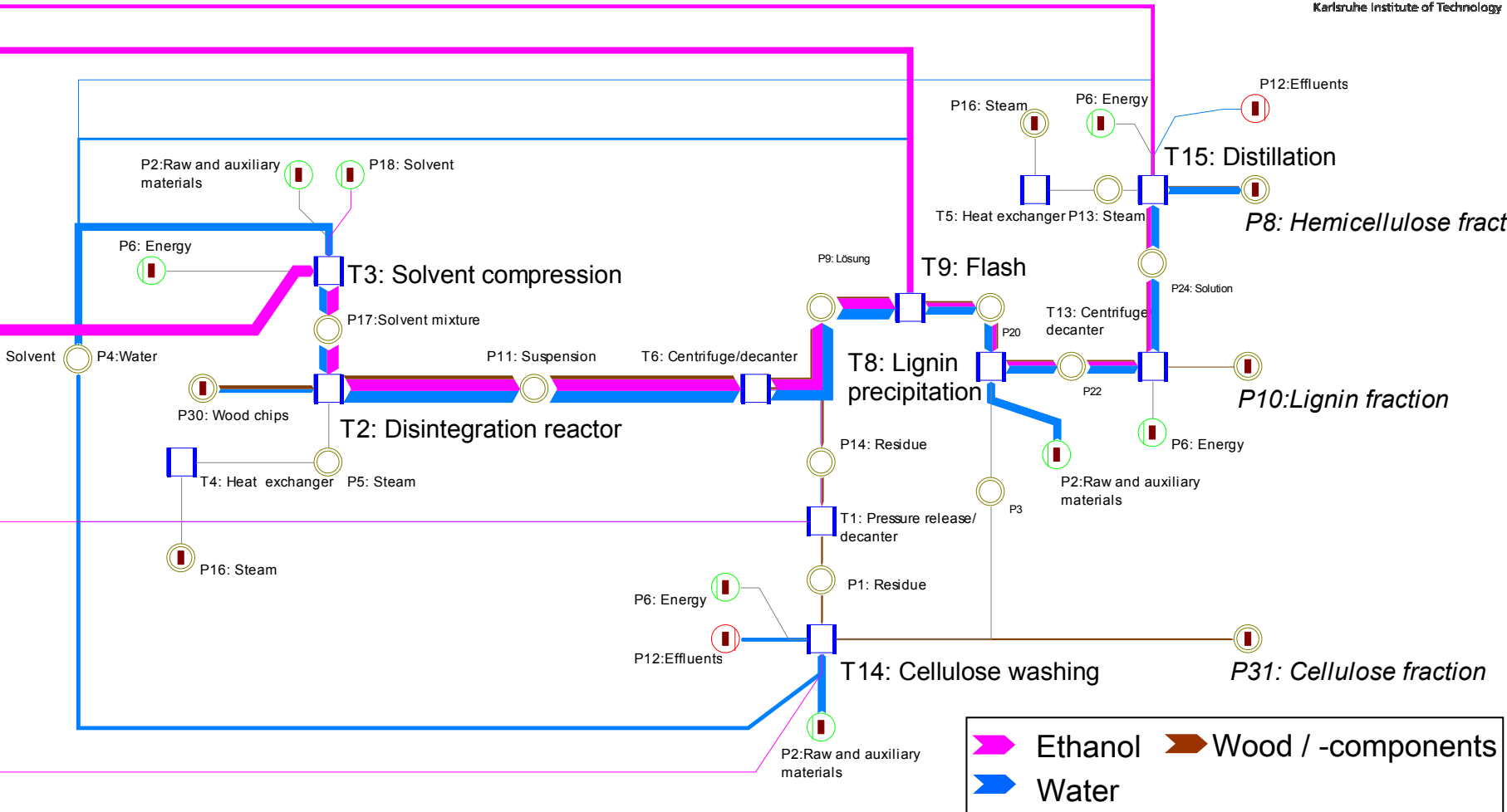
# Modeling of material and energy flows with Umberto

- Petri-net based software tool
- Specification of process steps along the whole value chain in different subnets



- Model calculations are carried out for different scenarios via parameter selection (e.g. different wood : solvent ratios)
- Input data for the model derived from literature, laboratory experiments, thermodynamic modelling with ASPEN Plus.

# Subnet „pulsing and separation of components“ (sankey diagram)



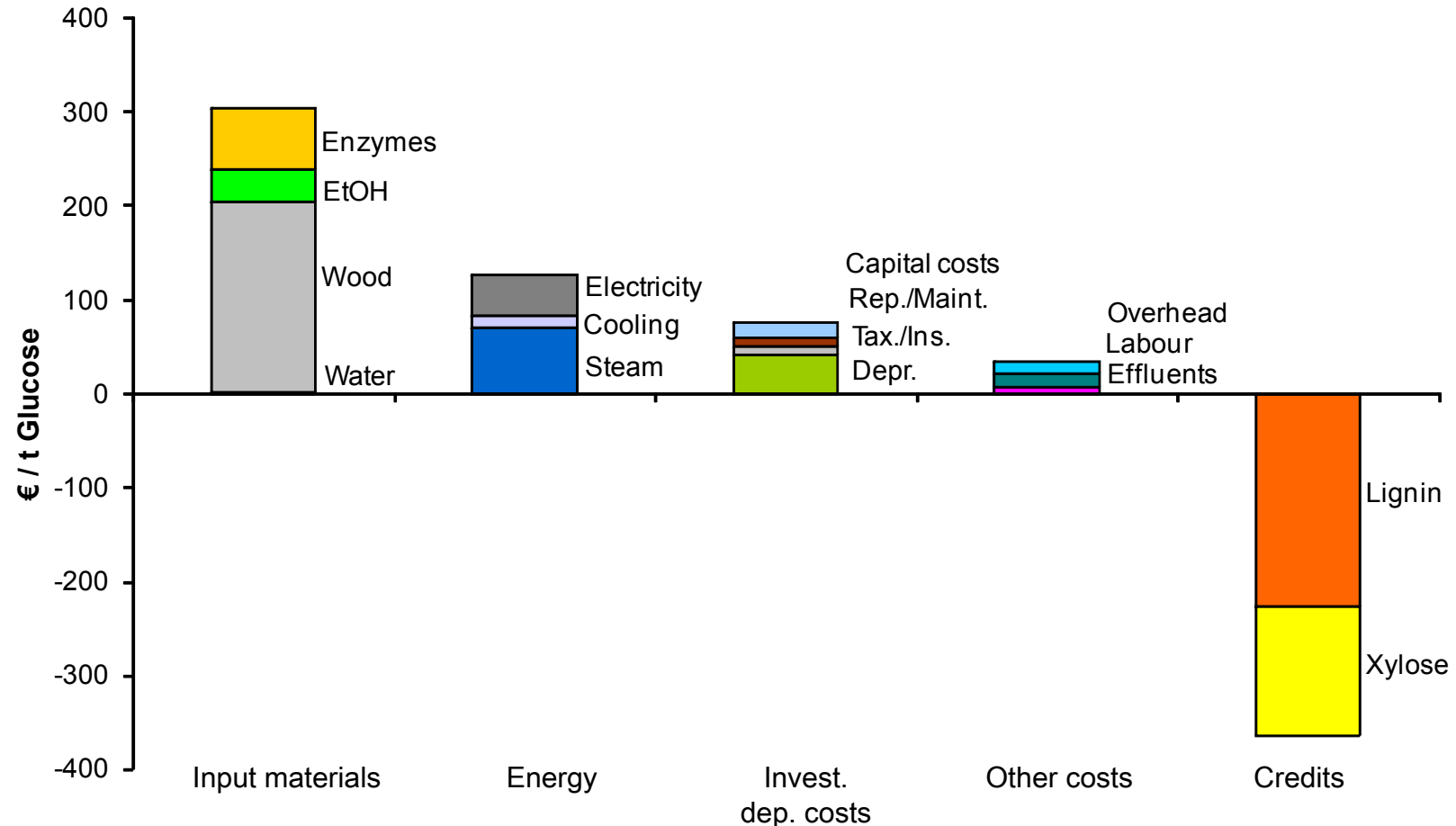
- High amounts of ethanol and water have to be recycled.
- Ethanol recovery via distillation: Key parameter regarding the energy demand

# Methodology for economic analysis

- Estimation of investments:
  - +/- 30% accuracy
  - Site infrastructure completely available and useable (outside battery limits neglected)
  
- Estimation of glucose production costs:
  - Variable costs and credits
    - Costs for raw and operating materials (wood chips, ethanol, water, enzymes)
    - Energy costs (electricity, steam, cooling)
    - Costs for sewage disposal
    - Credits for by-products (lignin as high grade product, xylose)
  - Investment related costs (depreciations, taxes and insurance, maintenance, costs of capital)
  - Costs for labour
  
- Costs for sales, administration and research are not yet determined

# Structure of costs and credits

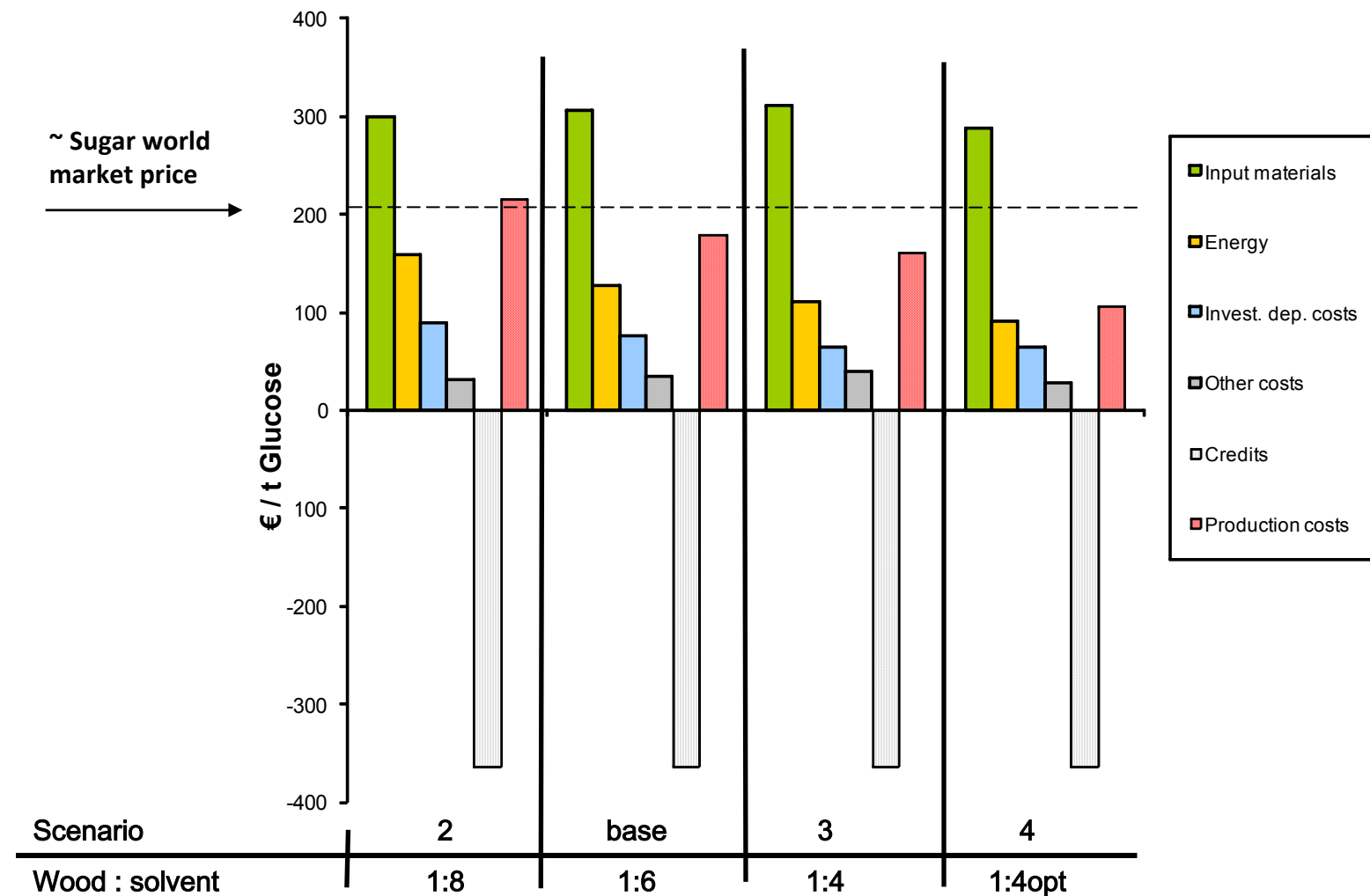
Base scenario (ratio wood : solvent = 1 : 6)



Highest influence on the amount of glucose production costs: Costs for wood chips and the credits for lignin as by-product

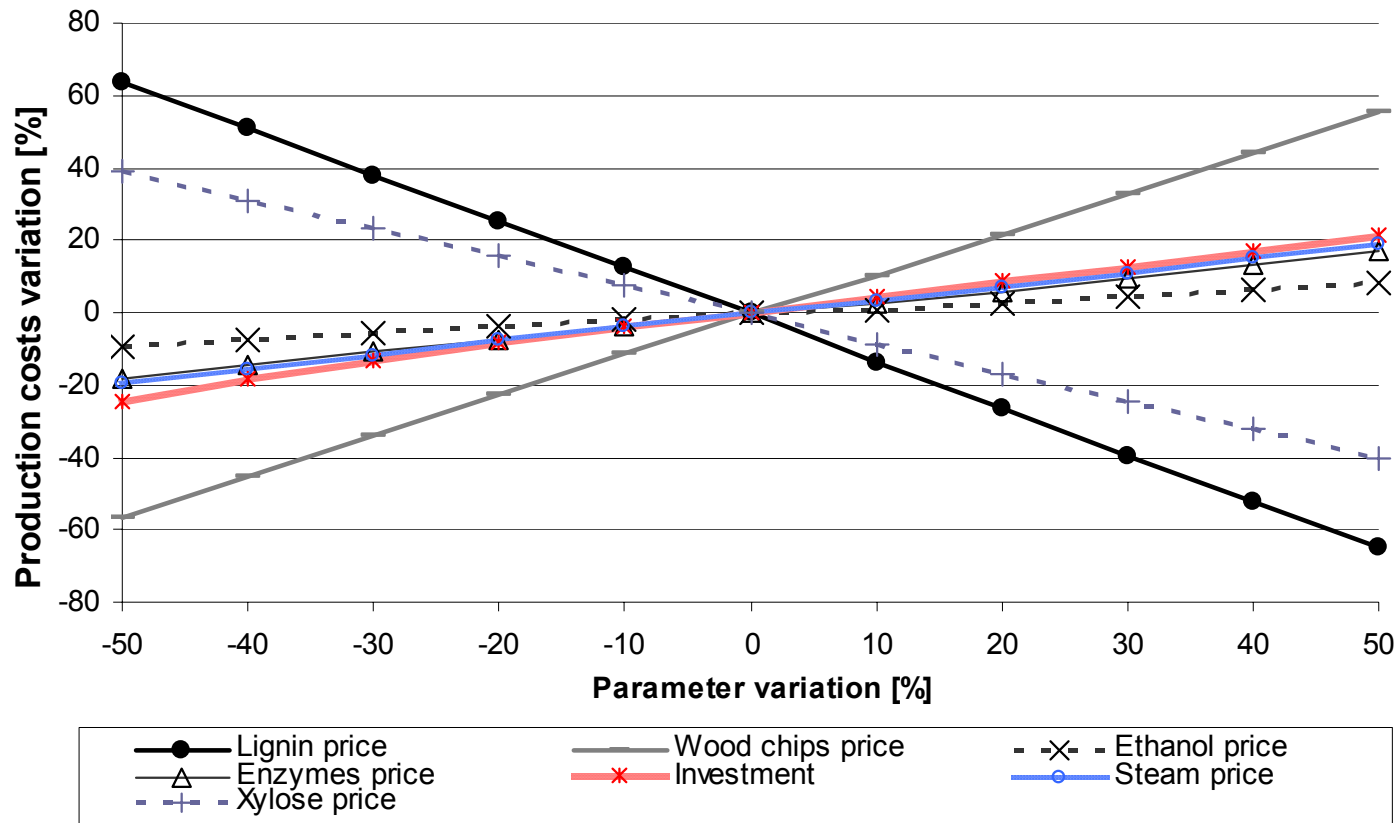
# Estimation of glucose production costs

- Comparison of different wood : solvent ratios
- Requirement for economic efficiency: production costs << sugar market price



# Sensitivity analysis

- Base scenario (ratio wood : solvent = 1 : 6)
- Influence of different prices on the glucose production costs

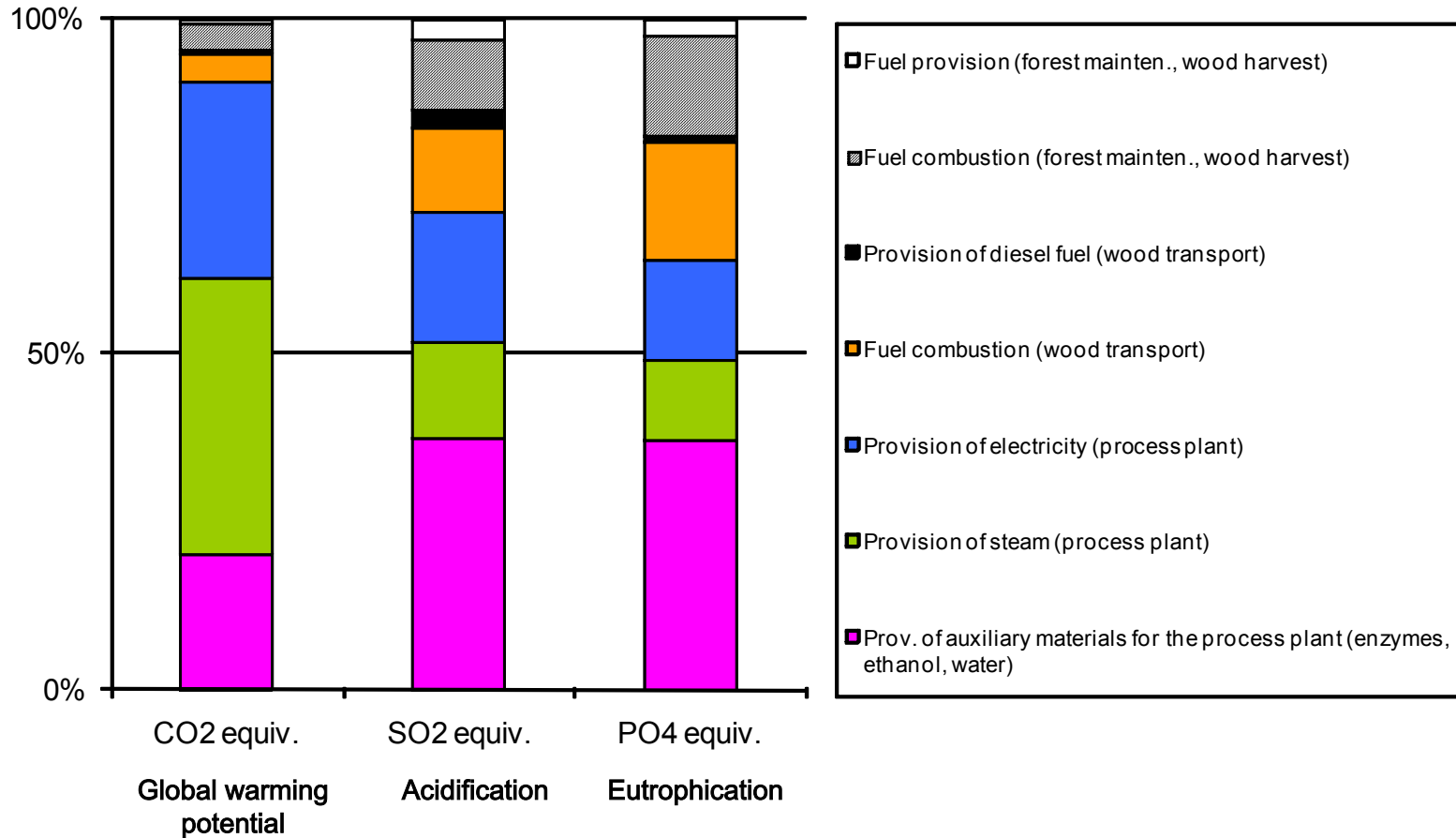


- Prices for wood chips and lignin mainly influence glucose production costs

- Methodology for life cycle assessment (LCA) according to the international standard DIN EN ISO 14040 and 14044
- Goal and scope definition and life cycle inventory (LCI) analysis
  - „Cradle to gate analysis“ including forest production (wood maintenance, wood harvest/chipping), wood transport and the biorefinery processes
  - Integration of supply chains for the provision of energy and operating materials (ecoinvent v2.0 LCI database)
- Selection of impact categories, e.g. global warming potential, acidification, eutrophication
- Life cycle impact assessment (assignment of LCI results to the corresponding impact categories and conversion to indicator values, e.g. CO<sub>2</sub> equivalents)

# Ecological assessment – Examples (1)

Determination of proportions of particular process steps to the emission equivalents of selected impact categories

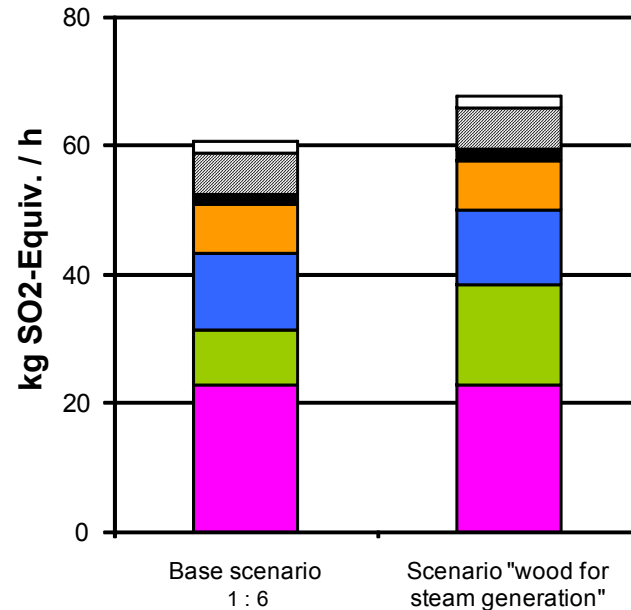
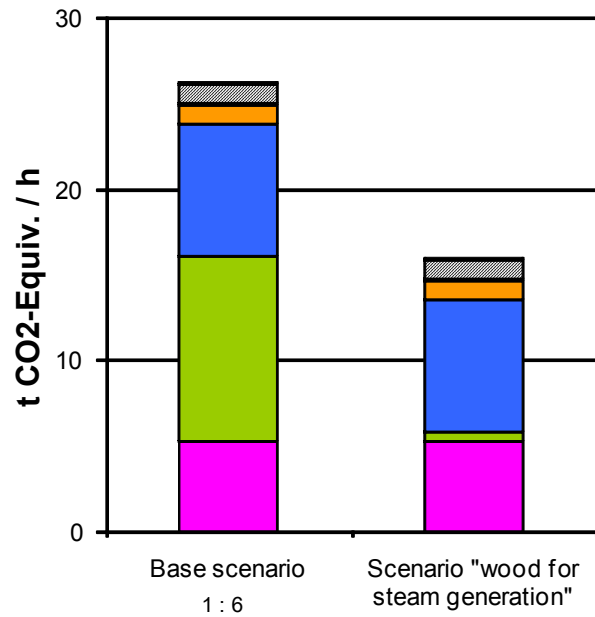


Uncertainties for contributions caused by enzymes production especially for PO<sub>4</sub>- equiv.



# Ecological assessment – Examples (2)

Comparison of CO<sub>2</sub>- and SO<sub>2</sub>- emission equivalents assuming different fuels for steam generation



- Prov. of auxiliary materials for the process plant (enzymes, ethanol, water)
- Provision of electricity (process plant)
- Provision of diesel fuel (wood transport)
- Fuel provision (forest mainten., wood harvest)

- Provision of steam (process plant)
- Fuel combustion (wood transport)
- Fuel combustion (forest mainten., wood harvest)

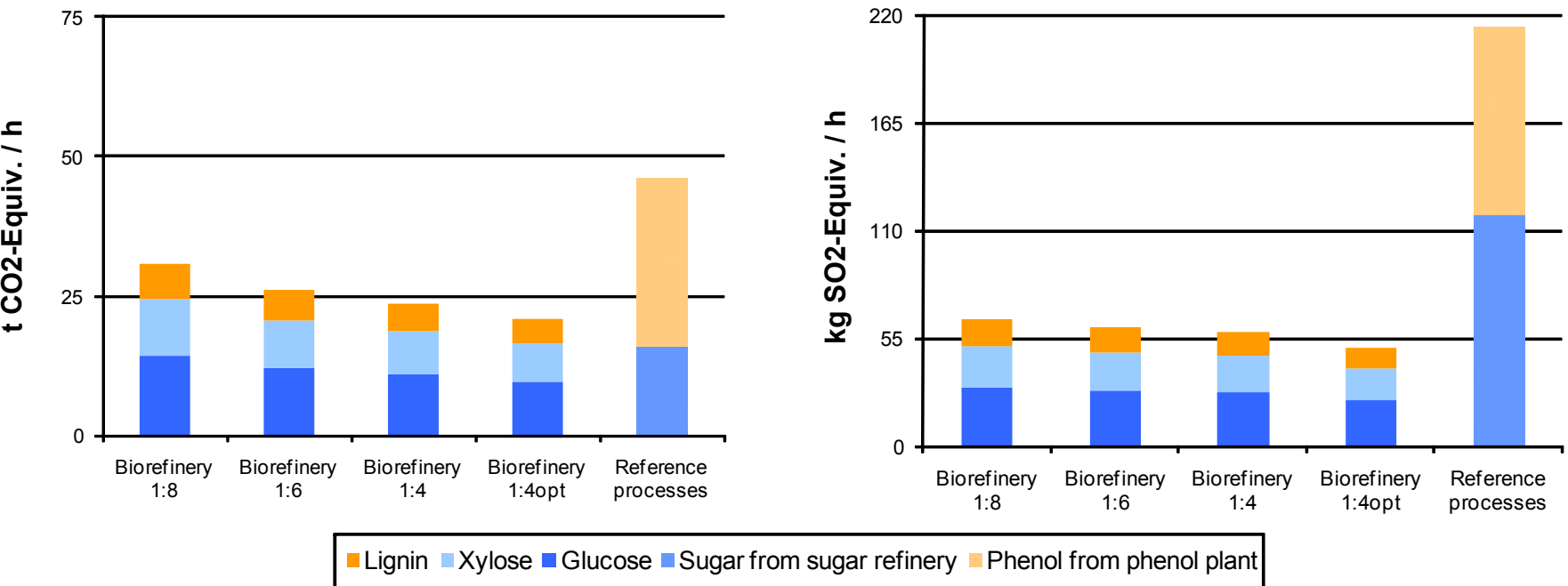
Wood combustion for steam generation lowers CO<sub>2</sub>- emission equivalents but elevates SO<sub>2</sub>-emission equivalents

# Ecological assessment – Examples (3)

Comparison of CO<sub>2</sub>- and SO<sub>2</sub>- emission equivalents of the biorefinery with the production of potential reference products<sup>1</sup>

Assumptions:

- Sugar from a sugar refinery as reference product for solute xylose and glucose
- Phenol from a phenol plant as reference product for lignin



Lower CO<sub>2</sub>- and SO<sub>2</sub>- emission equivalents for the biorefinery compared to selected reference processes

<sup>1</sup> Values for reference processes derived from the ecoinvent v2.0 LCI database

- Development of new concepts for the non-energetic use of biomass
- Modelling of mass and energy flows of a wood biorefinery along the whole value chain for different scenarios
- Early-stage techno-economic and ecological assessment for the identification of sustainable production processes
- Economic efficiency highly depends on prices for wood chips and the sales price for lignin
- Further improvement of the process design is necessary to enhance economic efficiency
- Steam and electricity generation are crucial for the extent of GHG emissions
- Analysis of different environmental impact categories may lead to different conclusions
- Further research is needed especially with respect to products utilization/processing
- Consideration of more detailed analysis of product streams

# Thank you for your attention



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GEFÖRDERT VOM



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